

4th International Workshop on Sample Environment at Neutron Scattering Facilities

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Spreadsheet Calculations for Sample Environment Problems

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Motivation

- **Learn**

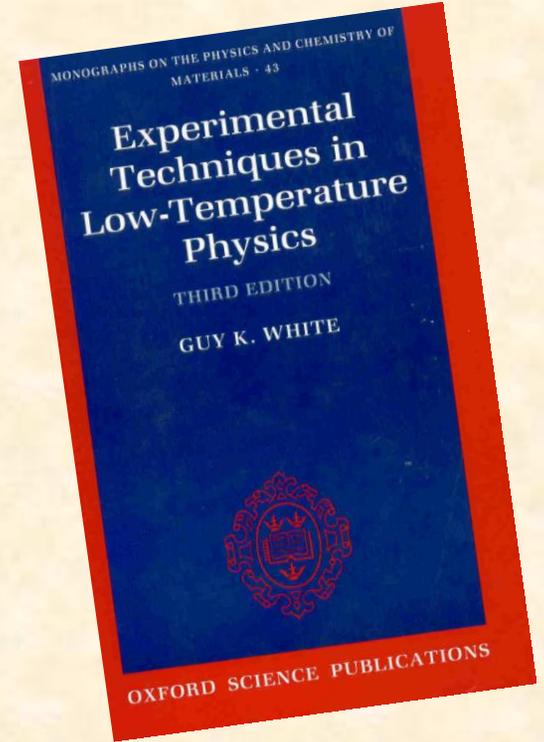
- How to apply fundamental principles to sample environment problems
- How to obtain useful quantitative models

- **Work smarter**

- Evaluate concepts before cutting metal
- Compare observed and calculated data to better understand system behavior

Starting Point

- **Classic reference guide**
 - Simple examples
 - Useful tables
- **Setup companion spreadsheets**

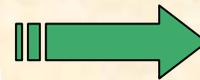


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APPENDIX

TABLE D
Some important physical functions (see Chapter XI)

T/θ	θ/T	C_v (J/mol K)	ρ/ρ_0 $(\alpha T^3 J_3)^\dagger$	ρ_i/ρ_0 $(\alpha T^3 J_3)^\ddagger$	W_i/W_∞ $(\alpha T^2 J_2)^\S$
(∞)	0	24.94	∞	∞	1.00
(10)	(0.1)	24.93	10.55	10.42	1.00
(5)	0.2	24.89	5.268	5.201	0.998
(2.5)	0.4	24.74	2.617	2.588	0.993
(2.0)	0.5	24.63	2.083	2.062	0.990
(1.667)	0.6	24.50	1.725	1.711	0.985
(1.25)	0.8	24.16	1.274	1.268	0.974
(1.0)	1.0	23.74	1.000	1.000	0.960
(0.833)	1.2	23.23	0.813	0.8186	0.943
(0.714)	1.4	22.66	0.678	0.6873	0.923
(0.667)	1.5	22.35	0.623	0.6341	0.913



Microsoft Excel - Cool Debye.xls

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D24

	C	D	E	F	G	H
20						
21			Debye Table		Sample	
22			theta/T	U-U ₀ /T	T(Fe)	U-U ₀ [J/mol]
23			0.2	23.1	2000	46200
24			0.4	21.38	1000	21380
25			0.6	19.76	667	13173
26			0.8	18.24	500	9120
27			1	16.81	400	6724
28			1.2	15.47	333	5157
29			1.35	14.54	296	4308
30			1.4	14.23	286	4066
31			1.6	13.07	250	3268
32			1.8	11.99	222	2664
33			2	11	200	2200

Problem 1: Cooling with Liquid Nitrogen and Helium

- **Need to cool a 10kg hunk of iron**
 - Initially at 293K
- **How much liquid helium required ...**
 - to cool to 4.2 K?
 - If pre-cooled to 77K with LN2?

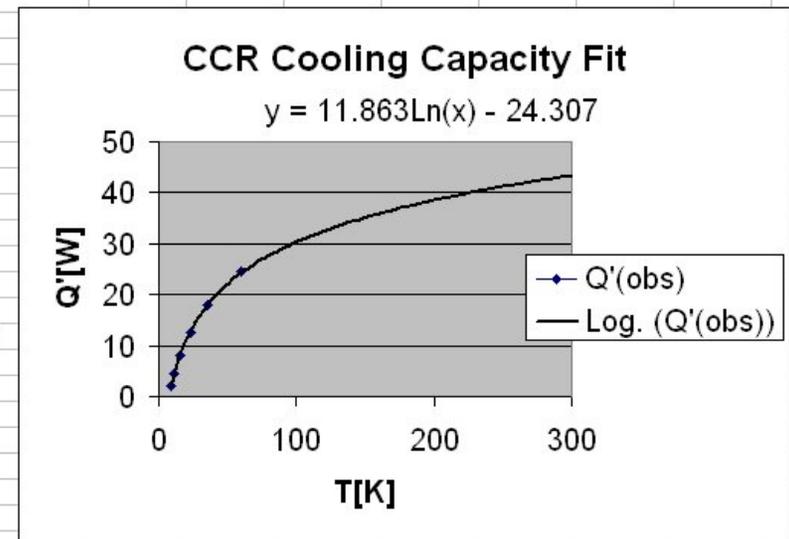
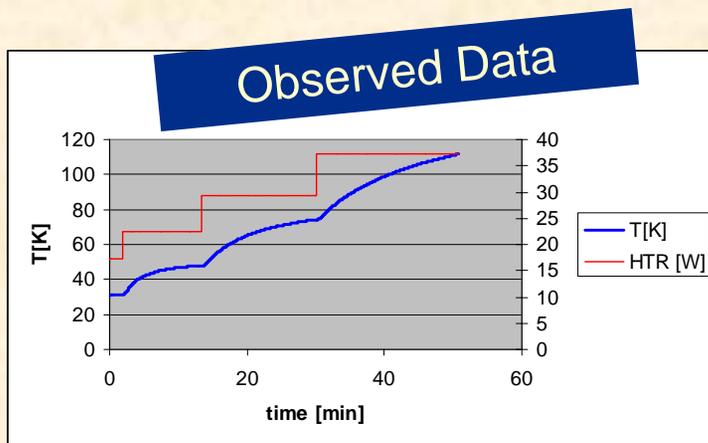
Problem 1: Cooling with Liquid Nitrogen and Helium

- Need to cool a 10kg hunk of iron
 - Initially at 293K
- How much liquid helium required ...
 - to cool to 4.2 K? **490 liters**
 - If pre-cooled to 77K with LN2?
 - **6 liters LN2**
 - **125 liters LHe**

	A	B	C	D	E	F	G	H	I
1	Cryogen Consumption Calculator								
2							Debye Table		
3	Material Spec			Calculate			theta/T	U-Uo/T	
4	mass [g]	10000					0.2	23.1	
5	Debye Temp	400		How many liters?			0.4	21.38	
6	molar mass	55.9		493.2			0.6	19.76	
7	Temperatures						0.8	18.24	
8	T(initial)	293					1	16.81	
9	T(final)	4.2					1.2	15.47	
10							1.35	14.54	
11	Cryogen spec						1.4	14.23	
12	latent heat	2.6					1.6	13.07	
13							1.8	11.99	
14	Reference						2	11	
15	Latent Heat of Vap. [J/ml]						2.2	10.08	
16	Helium	2.6					2.4	9.23	
17	Nitrogen	161					2.6	8.44	
18	Debye Temperatures [K]		g/mol				2.8	7.73	
19	Copper	310	63.5				3	7.07	
20	Aluminum	380	27				3.5	5.66	
21	Iron	400	55.9				4	4.53	

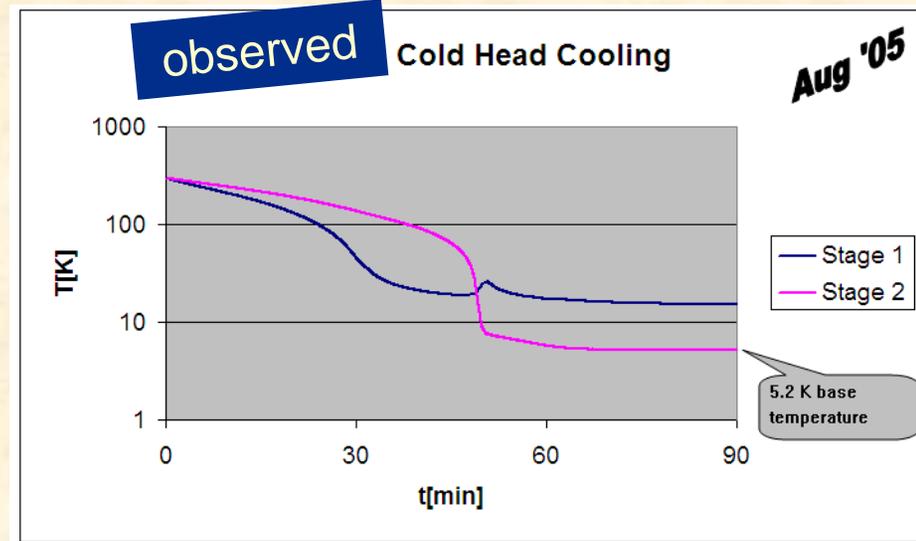
Problem 2: Cooling with CCR

- **2a: What is CCR cooling capacity?**
 - Temperature dependent
 - Vendor info limited
 - We need to measure it ourselves
 - Fit to function



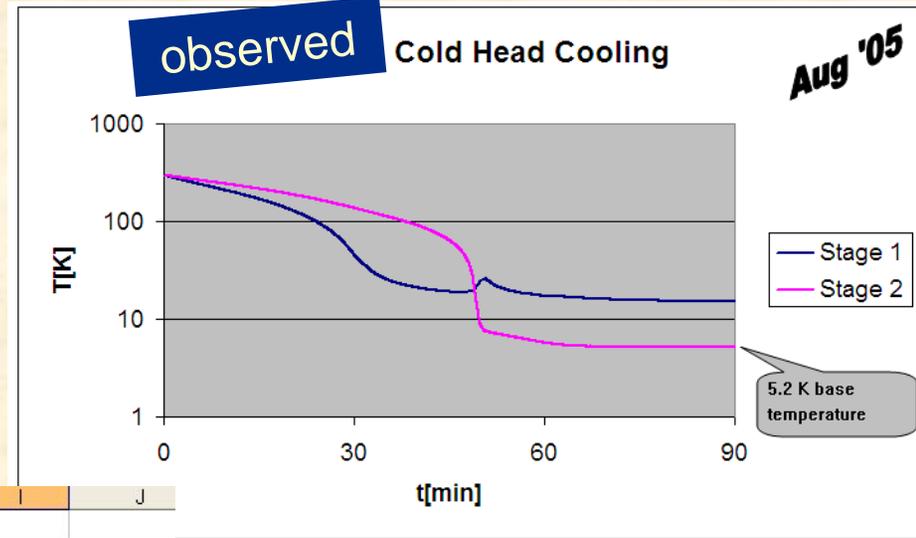
Problem 2b

- How long for the CCR to cool itself?



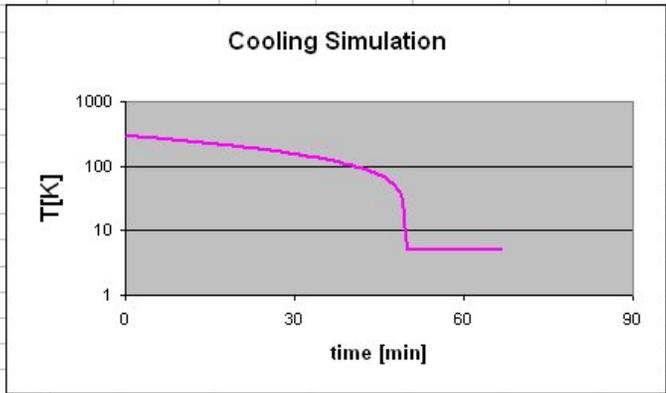
Problem 2b

- How long for the CCR to cool itself?



	A	B	C	D	E	F	G	H	I	J
1	Cooling CCR + Load									
2	Using fitted cooling capacity									
3	Debye heat capacity									
4										
5	23.27878261									
6	Material Spec									
7	Debye Temperature [K]	345								
8	Molar mass [g]	63.54								
9	Load mass [g]	0								
10	Self mass [g] est.	1500								
11	Fitted Cooling Capacity [W]									
12	$Q=A*\ln(T) - B$									
13		A	12							
14		B	24							
15										
16	Calculation Parameters									
17	Start Temperature	293								
18	time step [sec]	40.00								
19	Base temperature	5								

Calculate



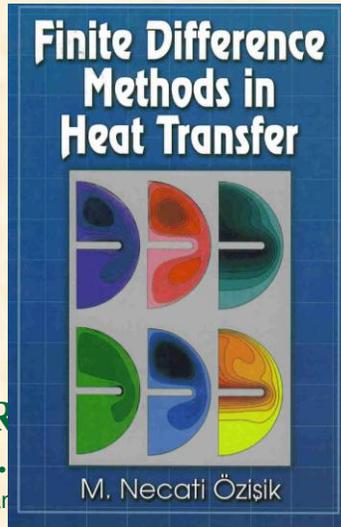
calculated

ref G. White	[J/mol*K]	T
theta/T	Cv	
0.2	24.89	1725
0.4	24.74	863
0.6	24.5	575
0.8	24.16	431
1	23.74	345
1.2	23.23	288
1.4	22.66	246
1.6	22.02	216
1.8	21.33	192

Reference	Debye	molar mass
Material		
Aluminium	426 K	26.97
Cadmium	186 K	112
Chromium	610 K	52
Copper	344.5 K	63.54

Calculation Notes

- **Finite difference approximation (FDA)**
- **First order differential equation**
- **Lots of shortcuts**
 - Using C_v from Debye table
 - Need C_p , but C_v is close and easy
 - Least accurate (1st order) FDA
- **Good reference**



Temperature $T(t) \rightarrow T_j \quad j = 0, 1, 2 \dots N$

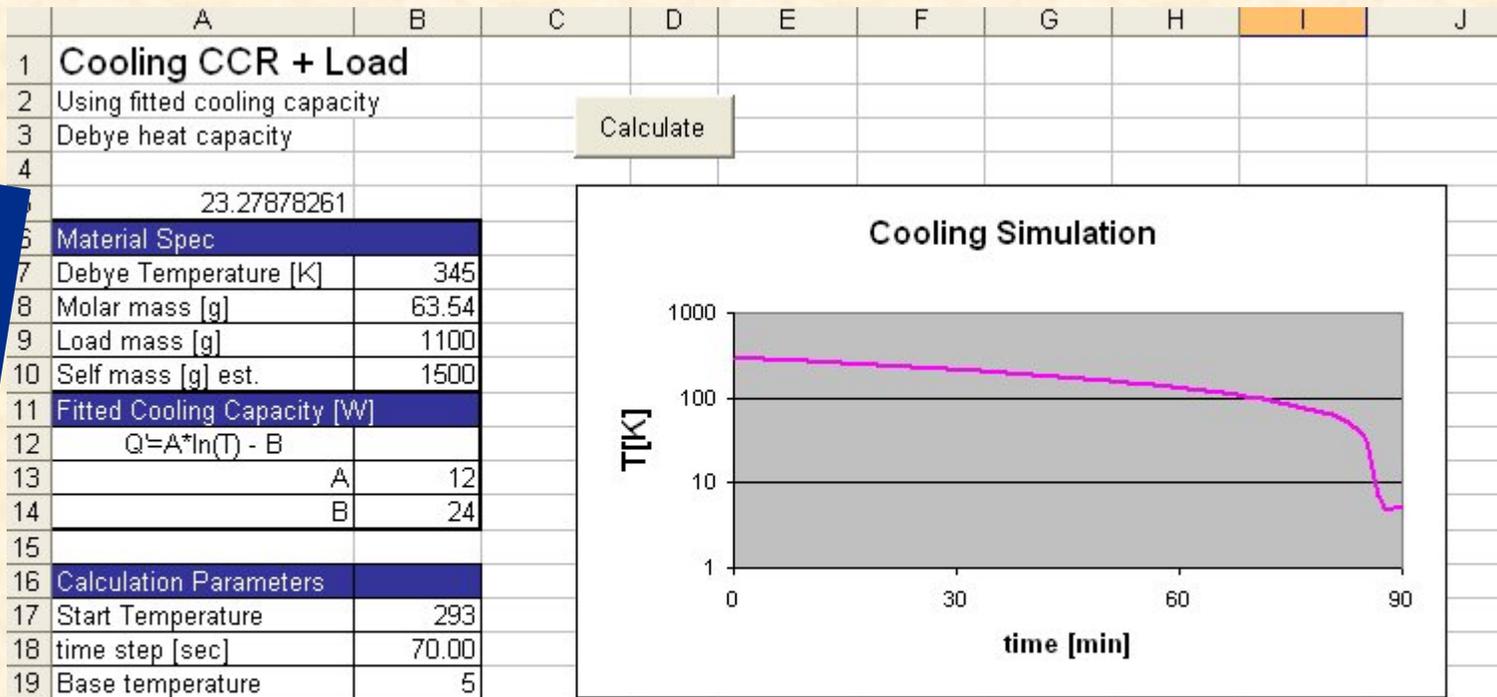
Similarly \dot{Q}_j, C_j (cooling power, heat capacity)
 $n = \text{number of moles}$

$$T_{j+1} = T_j - \frac{\Delta t \dot{Q}_j}{n C_j}$$

Problem 2c

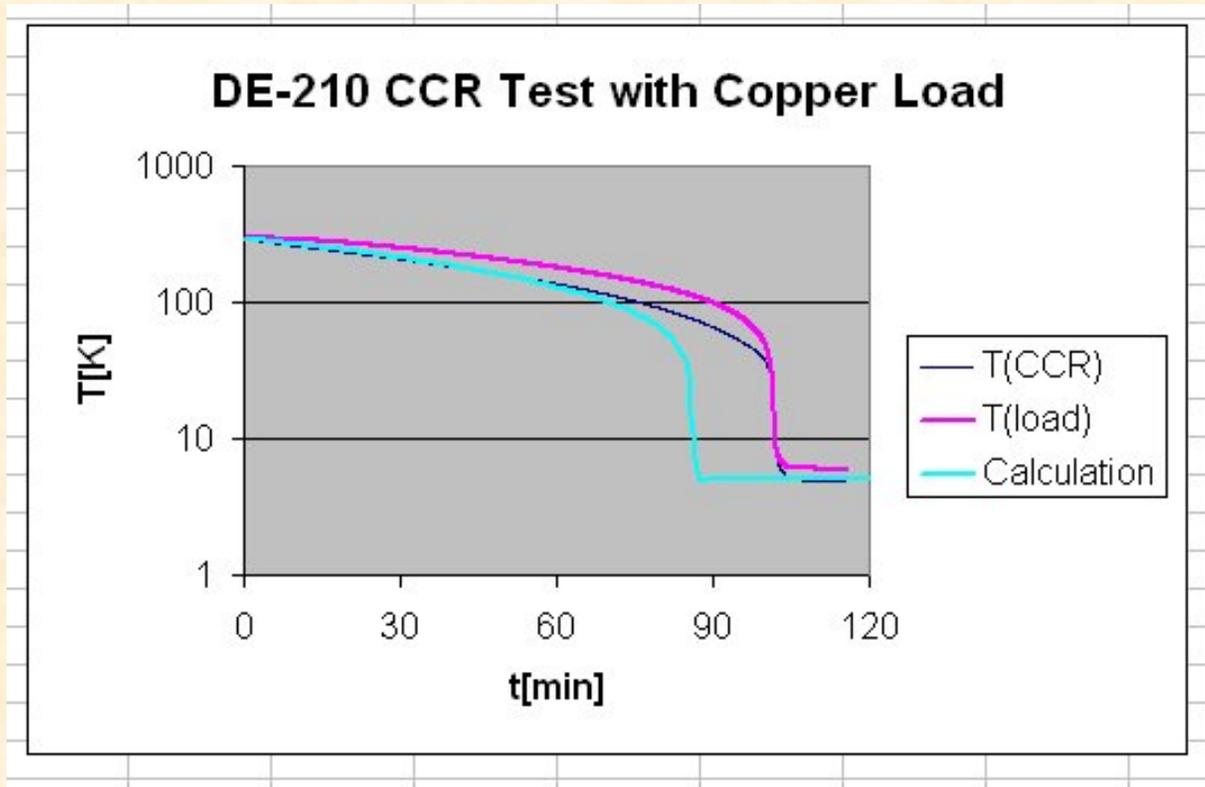
- Now attach a load to CCR
 - 3 pounds of copper
 - Simulate “SMASH rig” cold link

Calculation predicts 90 minute cool down



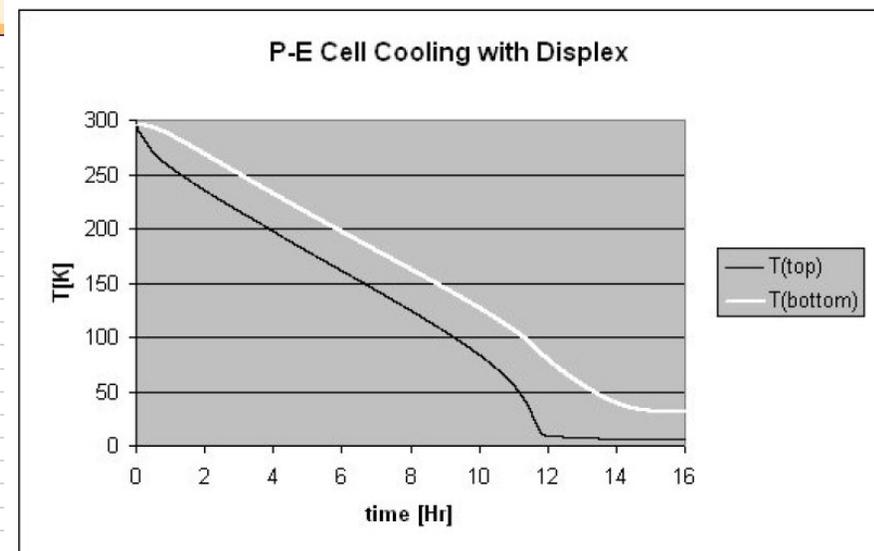
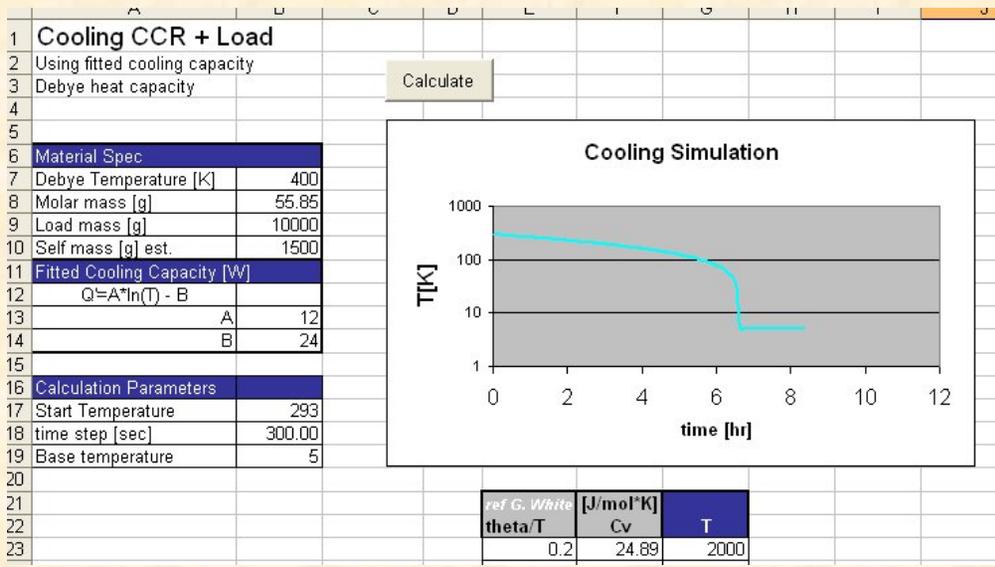
Problem 2c

- Test result gives 100 minutes



Problem 2d: Cool Something Bigger

- **Massive anvil pressure cell**
 - Paris-Edinburg Cell (model VX-2)
 - 25-pound hunk of steel!
- **Is it feasible to cool using CCR?**
 - Within a day
 - To 77K or lower

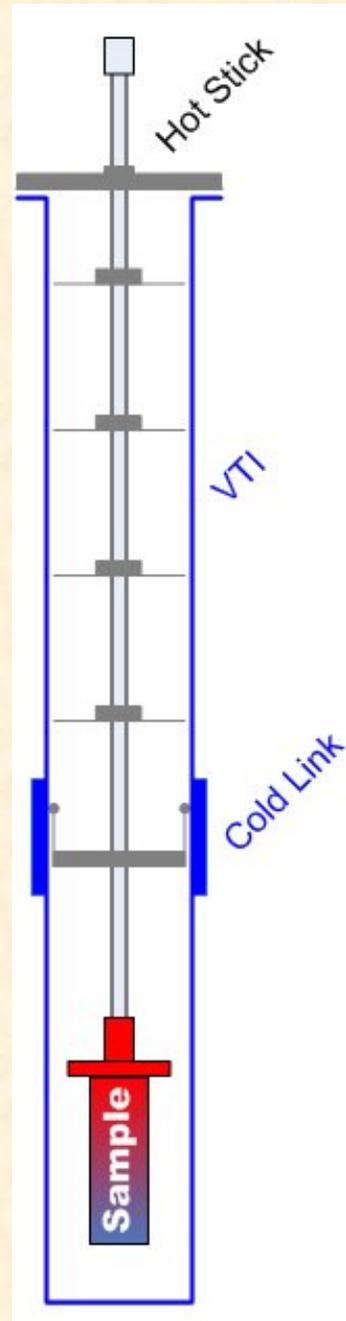


Problem 2d

- **Factor of two discrepancy between calculated and observed**
- **But calculation gave the right answer**
 - Yes, it is feasible

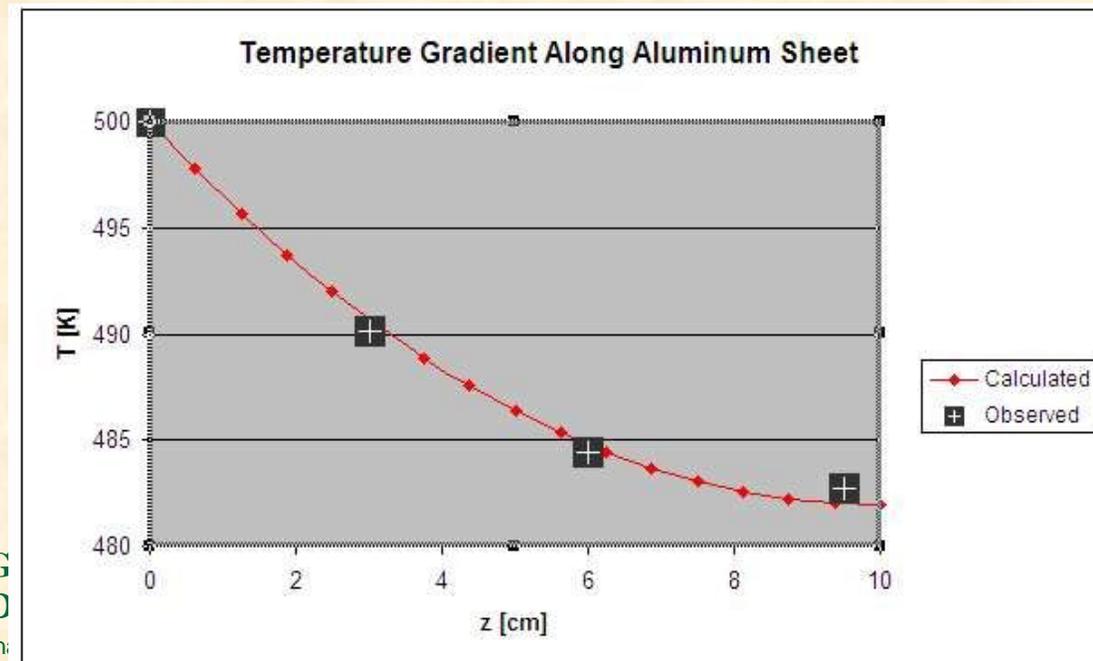
Problem 3: Hot Stick

- **Top-loading cryostat**
 - VTI range: 2 to 300 K
- **Hot stick reaches 600 K**
 - Different high and low temperature operating modes
 - Exchange gas for low temperature
 - Evacuated VTI for high temperature
- **We are concerned about temperature gradients in high temperature mode**



Calculate Gradient

- **Simplified scenario**
 - Flat sheet of aluminum
- **Setup comparable test**
- **Use results as a guide**



Calculation Notes

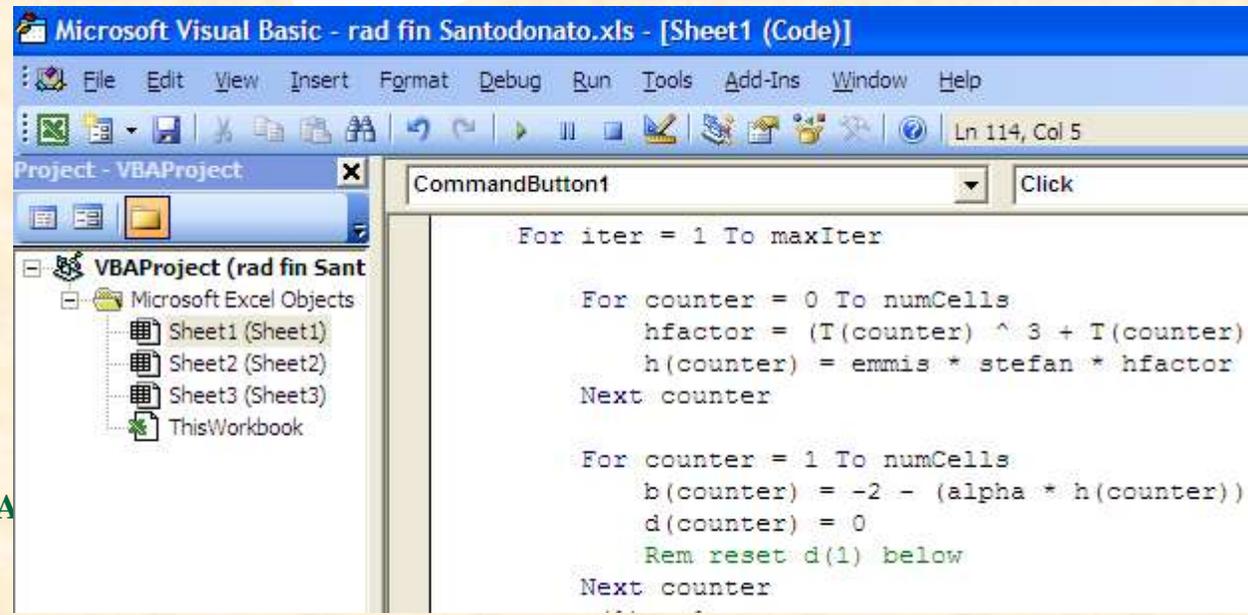
- **Setup like fin problem**
 - T-dependent “h”
 - Iterate, update h
- **Use “VBA” routine in spreadsheet**

88 FINITE DIFFERENCE METHODS

$$\frac{d}{dx} \left[A(x) \frac{d\theta(x)}{dx} \right] - \left(\frac{h}{k} \right) \frac{da(x)}{dx} \theta(x) = 0$$

where

- $A(x)$ = cross-section area normal to the x axis at the location x
- $a(x)$ = lateral surface area between $x=0$ and x
- h = heat transfer coefficient
- k = thermal conductivity of fin material
- $\theta(x) = T(x) - T_\infty$
- T_∞ = temperature of the ambient fluid.



The screenshot shows the Microsoft Visual Basic editor for a spreadsheet. The title bar reads "Microsoft Visual Basic - rad fin Santodonato.xls - [Sheet1 (Code)]". The menu bar includes File, Edit, View, Insert, Format, Debug, Run, Tools, Add-Ins, Window, and Help. The toolbar contains various icons for file operations and execution. The Project - VBAPROJECT window shows a tree view with "VBAProject (rad fin Sant)" containing "Microsoft Excel Objects" with "Sheet1 (Sheet1)", "Sheet2 (Sheet2)", "Sheet3 (Sheet3)", and "ThisWorkbook". The CommandButton1 window shows a "Click" event procedure with the following VBA code:

```
For iter = 1 To maxIter

    For counter = 0 To numCells
        hfactor = (T(counter) ^ 3 + T(counter)
        h(counter) = emmis * stefan * hfactor
    Next counter

    For counter = 1 To numCells
        b(counter) = -2 - (alpha * h(counter))
        d(counter) = 0
        Rem reset d(1) below
    Next counter
```

Summary

- **Rough calculations sometimes roughly agree with observed data**
 - No need for exact match
 - Just looking for guidelines
- **Gain a better understanding of sample environments by implementing both ...**
 - Rigorous equipment testing
 - Quantitative analysis

Acknowledgements

- **SNS Student Intern**
 - Rachel Morris
- **SNS Sample Environment Team**
 - L. Walker, B. Hill, J. Wenzel & R. McPherson
- **References**
 - Guy K. White, “Experimental Techniques in Low Temperature Physics”, Oxford University Press
 - M. Necati Ozisik, “Finite Difference Methods in Heat Transfer”, CRC Press (1994)